

Atmospheric Carbon Dioxide Capture Technology



Joey Keith Parkerson
jkparker@olemiss.edu

The Agenda

- The Twofold Situation
- Overview of Atmospheric CO₂ Capture Technology
- What to do with all the CO₂?
- Final Comments and Conclusions

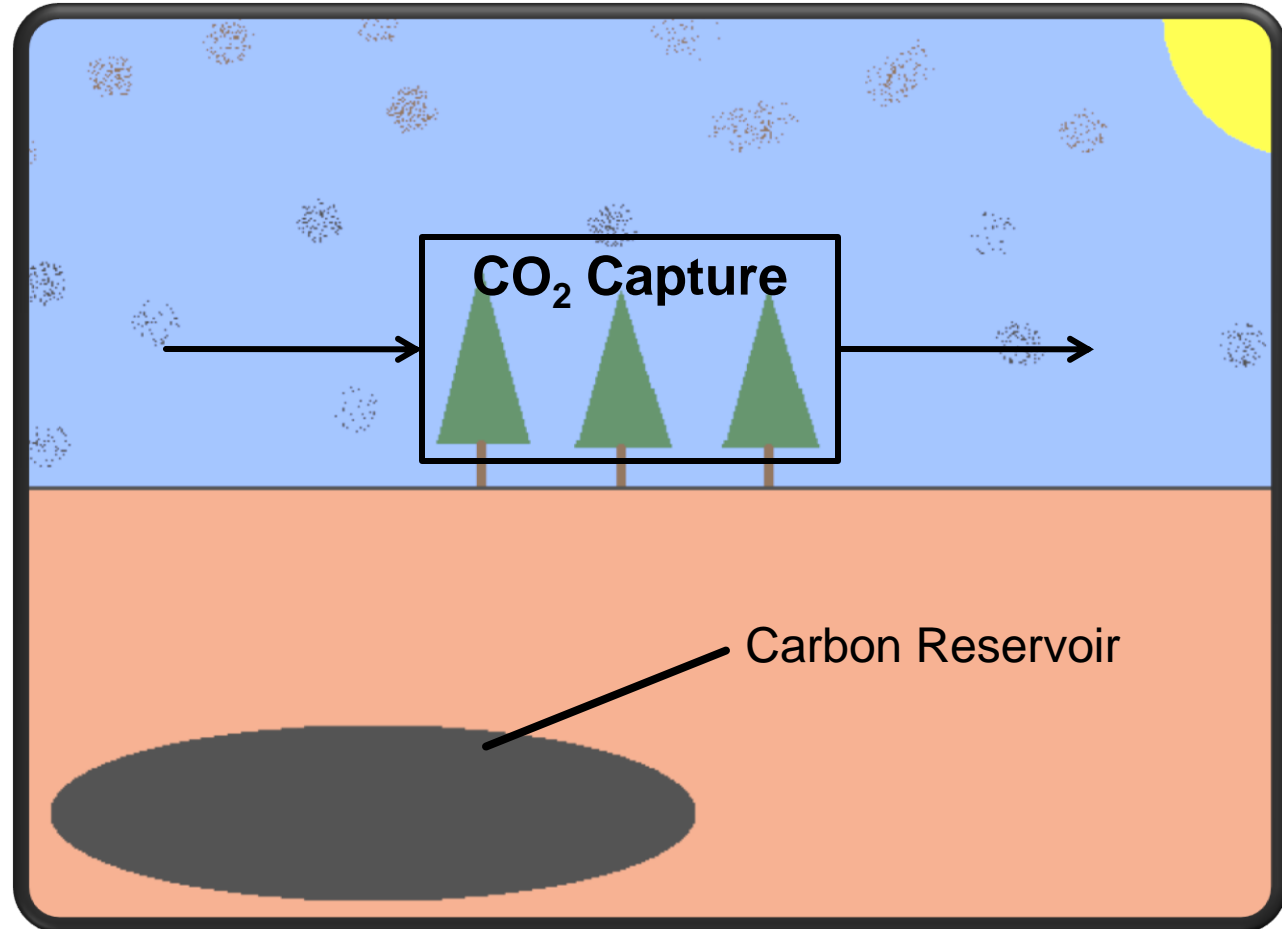


The Situation



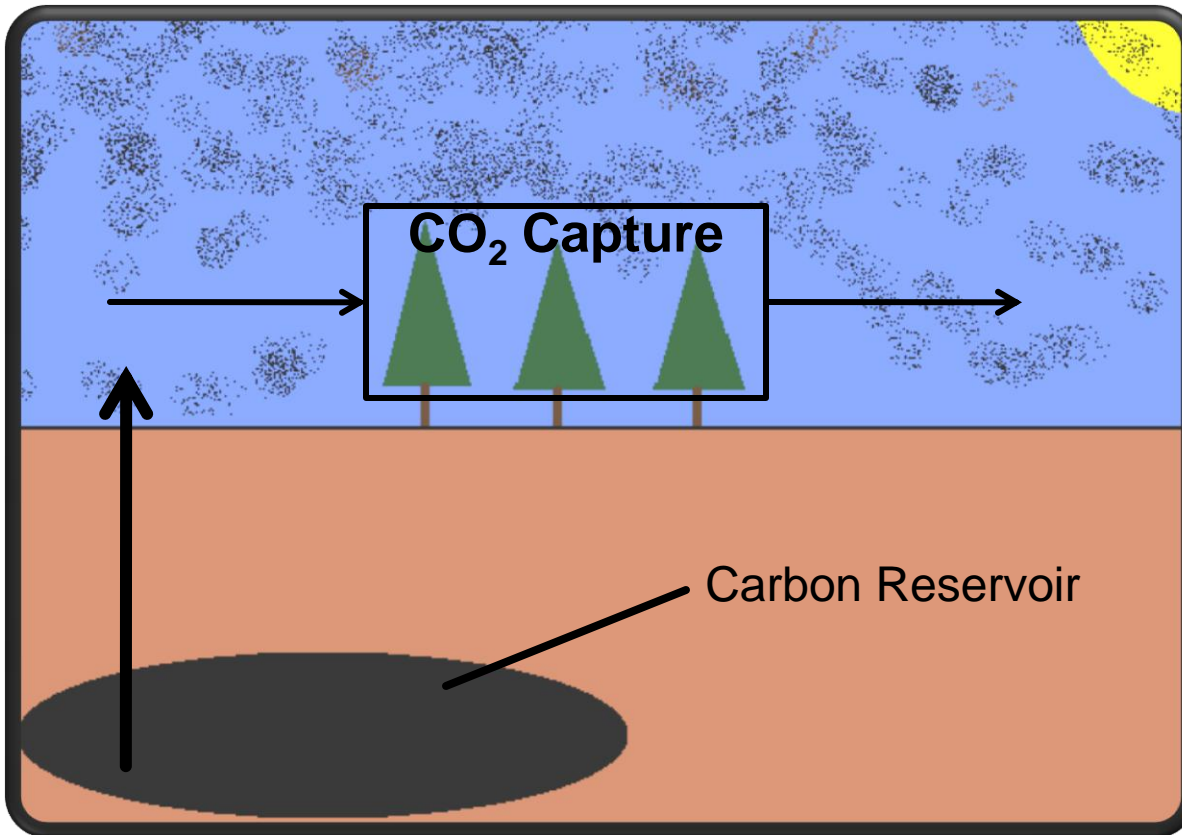
- Constant levels of CO₂ in atmosphere
- Maintains Temperature

Fixed Amount of Carbon in Process



The Situation

Mass Balance Problem!



System can't handle the extra load; thus, Global Warming becomes an issue!


The Situation

- Problem is two-fold:
 - Must solve CO₂ emissions problem
 - Must find viable future energy source
- Challenges to Reducing CO₂ emissions:
 - Non CO₂ sources are unlikely to displace fossil fuels at substantial levels
 - Coal and other fossil fuels will remain as major sources of energy regardless of the price issues
 - Coal is abundant



What if there was a system that solved ALL of these problems simultaneously?

The Technology

Dilute state (CO₂ at 360 ppm)  Concentrated state (CO₂ at > 90%)
P₀ = 3.6 x 10⁻⁴ atm P = 1 atm

Lower limit necessary to separate CO₂ from air given by energy needed to overcome free energy of mixing:

$$\Delta G = RT \ln \left[\frac{P}{P_0} \right]$$

$$\Delta G = 20 \text{ kJ/mol} = 1.7 \text{ GJ/tC}$$

The Technology

- What is Atmospheric Carbon Dioxide Capture?
 - The process of separating CO₂ from air at atmospheric conditions and delivering a pure stream of CO₂.

- Atmospheric Carbon Capture Methods
 - Sorbent Separation Methods
 - Na/Ca Capture - proven technology on small scale
 - GRT has Proprietary Sorbent
 - Ca(OH)₂
 - Electrochemical Separation - research in progress
 - Biomass
 - Metal-carbonate production

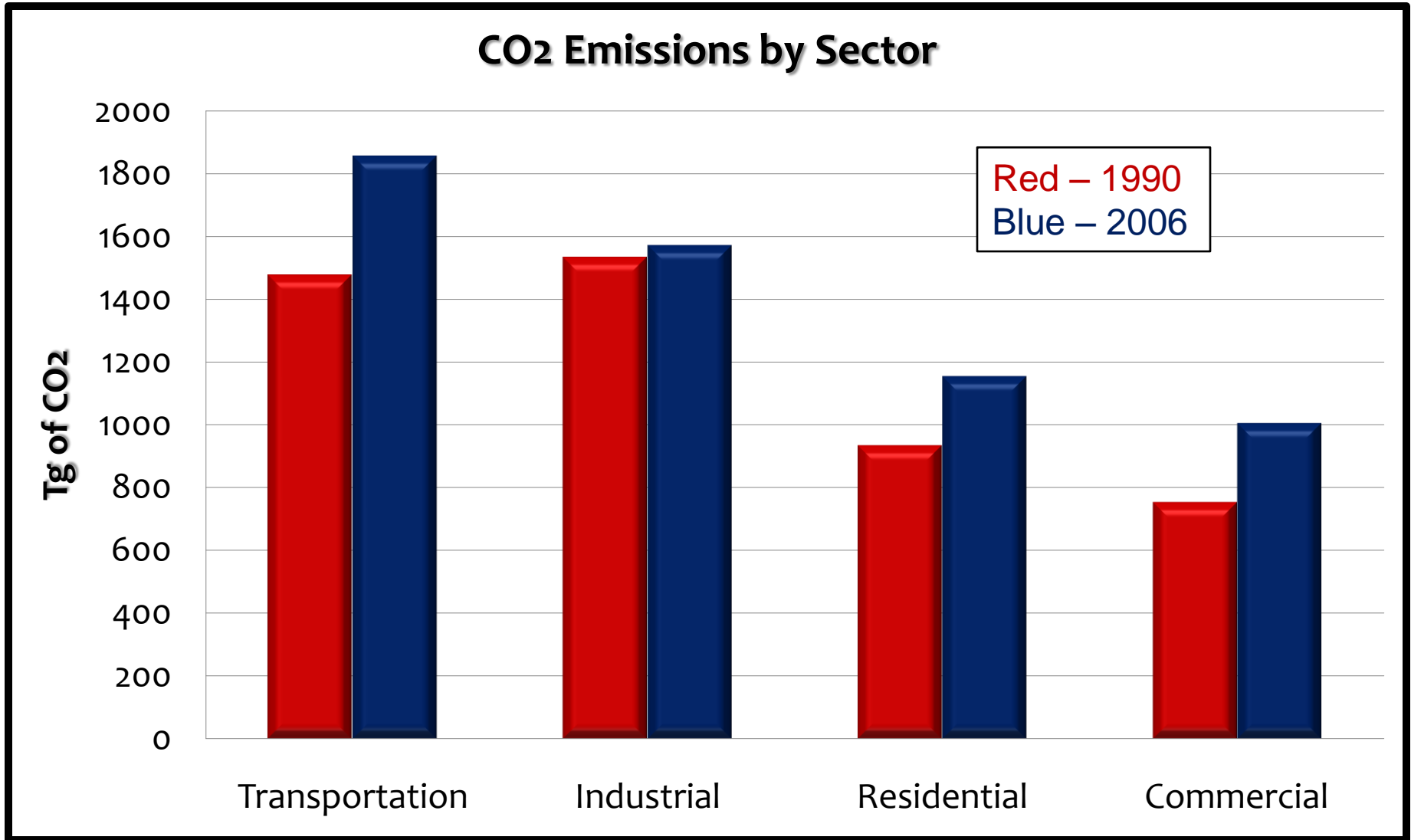
The Technology

Advantages

- Can not only provide “zero emissions energy” but also begin to remove the current buildup of CO₂
- Does not immediately make existing energy and transportation infrastructure obsolete
- No need for pipeline ~ atmosphere can serve as temporary storage and transport system
- Collects CO₂ after the fact from ANY SOURCE



The Situation



Data: US Environmental Protection Agency – Feb. 2008

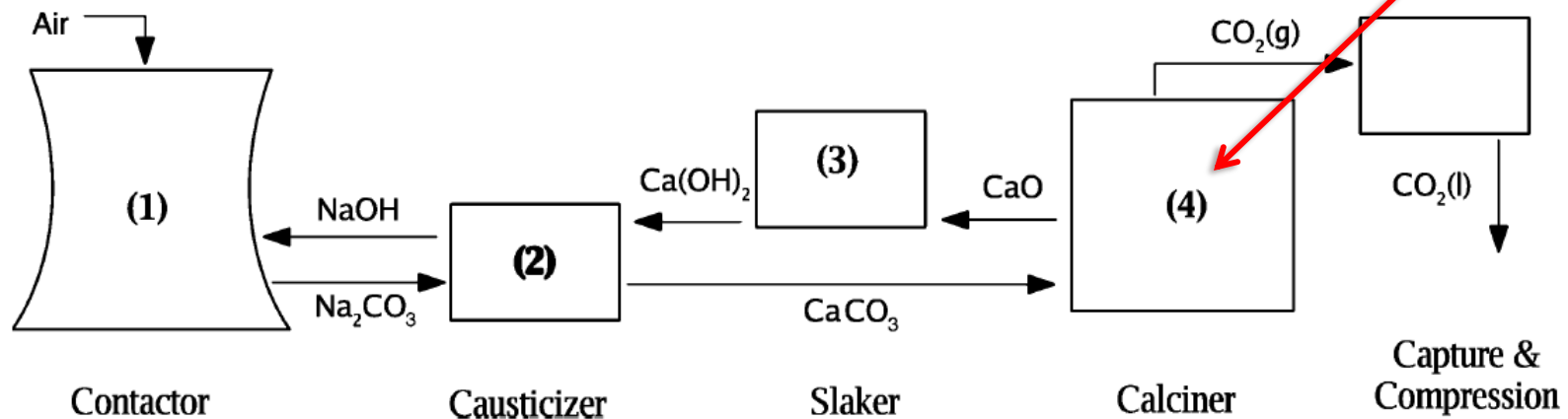
The Technology

Chemistry of Na/Ca capture system

| Reaction | Enthalpy of reaction ^a , ΔH° | |
|---|--|-------|
| | kJ/mol-C | GJ/tC |
| (1) $\text{CO}_2(\text{g}) + 2\text{Na}^+ + 2\text{OH}^- \rightarrow \text{CO}_3^{2-} + \text{Na}^+ + \text{H}_2\text{O}$ | -110 | -9 |
| (2) $\text{CO}_3^{2-} + \text{Ca}^{2+} \rightarrow \text{CaCO}_3(\text{s})$ | 12 | 1 |
| (3) $\text{CaO}(\text{s}) + \text{H}_2\text{O}(\text{l}) \rightarrow \text{Ca}^{2+} + 2 \text{OH}^-$ | -82 | -7 |
| (4) $\text{CaCO}_3(\text{s}) \rightarrow \text{CaO}(\text{s}) + \text{CO}_2(\text{g})$ | 179 | |

^aDerived from Weast (2003).

Lower Bound

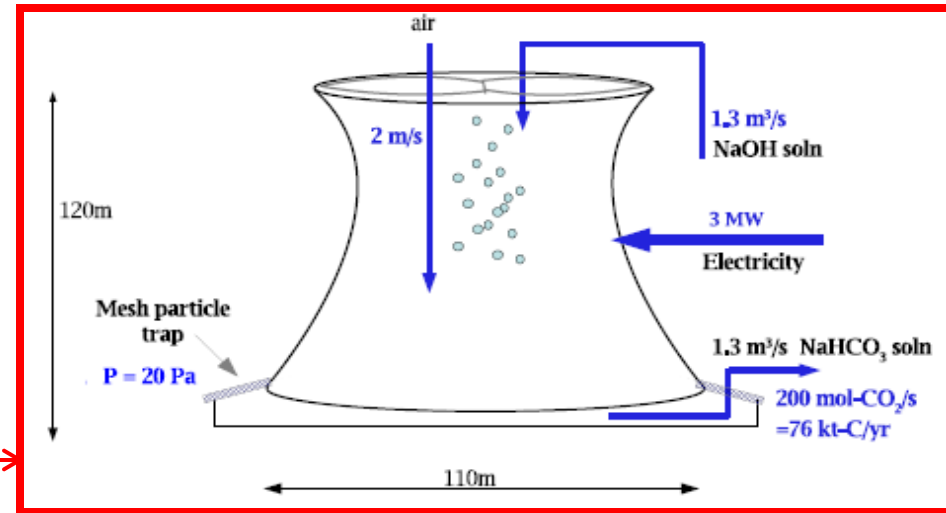


The Technology

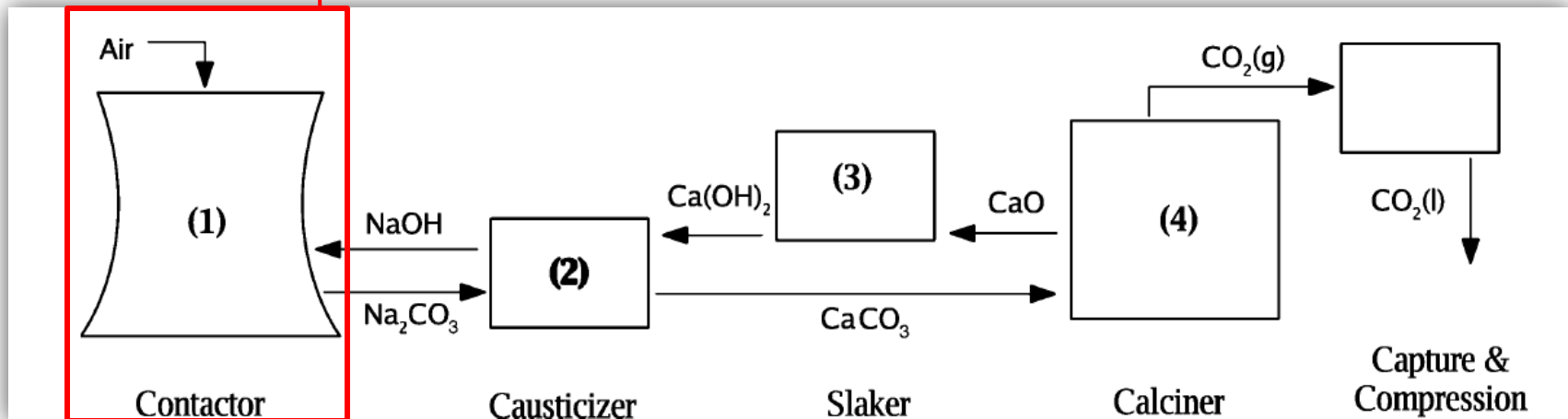
Contactor



- Captures CO₂ from Air
- Modeled as modified cooling tower
- Large capital cost



Stolaroff, Lowry, and Keith; CO₂ Capture from Air; March 2005



The Technology

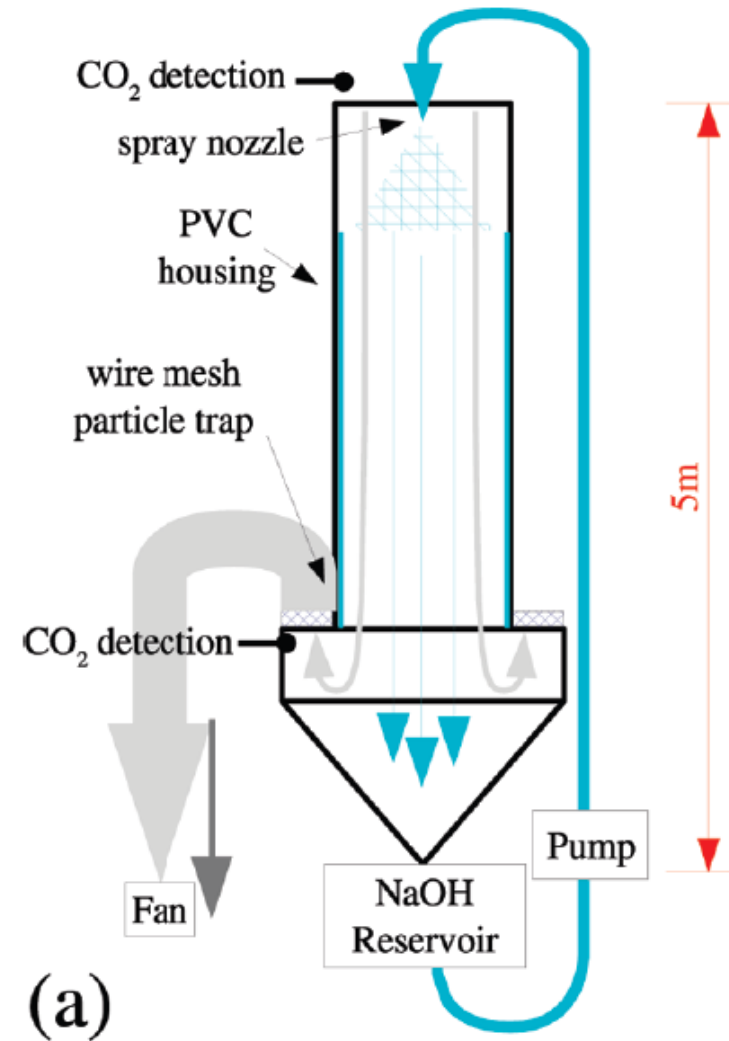
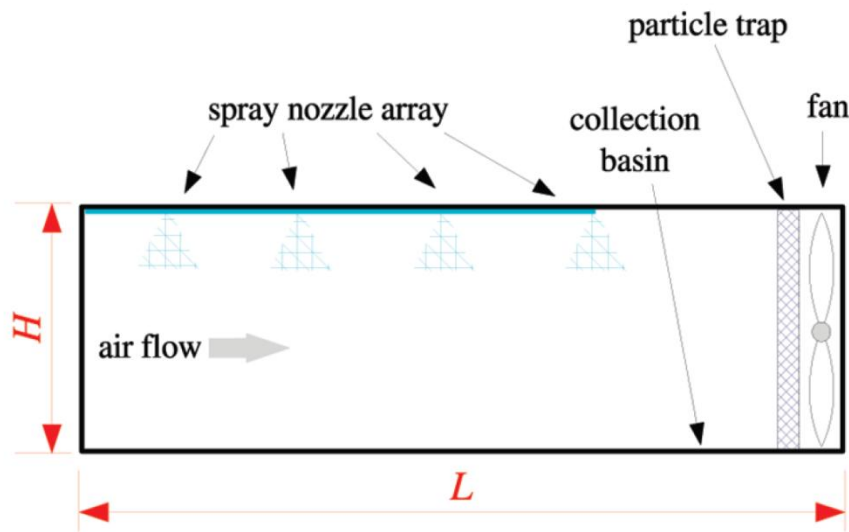
NaOH spray tower air capture unit: key parameters

| Parameter | Value | Motivation |
|---|---------------------|--|
| Tower diameter | 110 m | Equal to cooling tower |
| Tower height | 120 m | Equal to cooling tower |
| Air velocity | 2 m/s | Reasonable value ^a |
| CO ₂ capture efficiency from air | 50% | Reasonable value ^b |
| Mean drop diameter | 0.7 mm | Spray distribution from a hollow-cone spray nozzle |
| NaOH concentration in solution | 3–6 mol/l | Adjusted to minimize evaporative loss based on local climate. |
| Carbonate captured per pass ^b | 0.2 mol/l | Based on numerical model of falling drops |
| Solution flow rate | 1 m ³ /s | Fixed by above parameters |
| Pressure drop accross tower ^b | 22 Pa | Based on numerical model of falling drops; excludes wall friction. |
| Electricity use | 1.4 MW | Based on 75% fan and 85% pump efficiency |
| Carbon capture rate | 76000 tC/yr | Fixed by above parameters |
| Capital cost ^c | \$12 million | (Cooling tower cost) × 1.5 ^c |
| Operation and maintenance cost | 400,000 \$/yr | Conservative guess |

The Technology

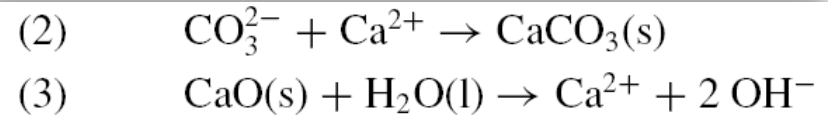
Alternative Suggested Contactor

- Many of these housed in larger unit

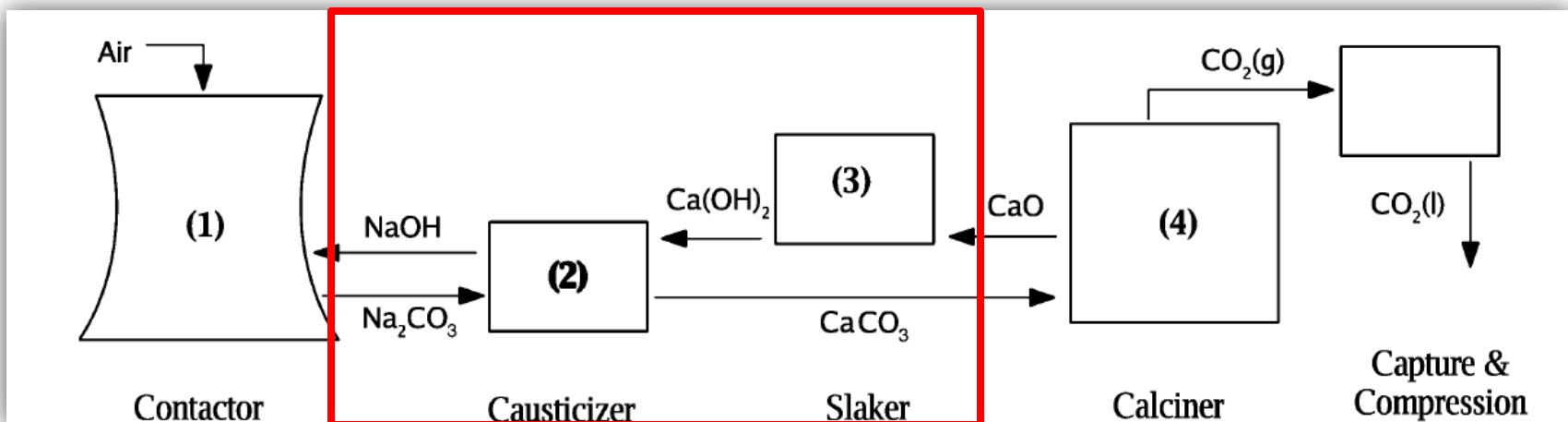


The Technology

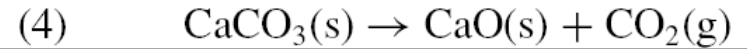
Causticizer and Slaker



- Modeled as one unit: similar to Kraft Process
- Part of Na/Ca chemical loop
- Causticizer
 - swaps Na with Ca on “bottom pass”
 - Swaps Ca with Na on “top pass”

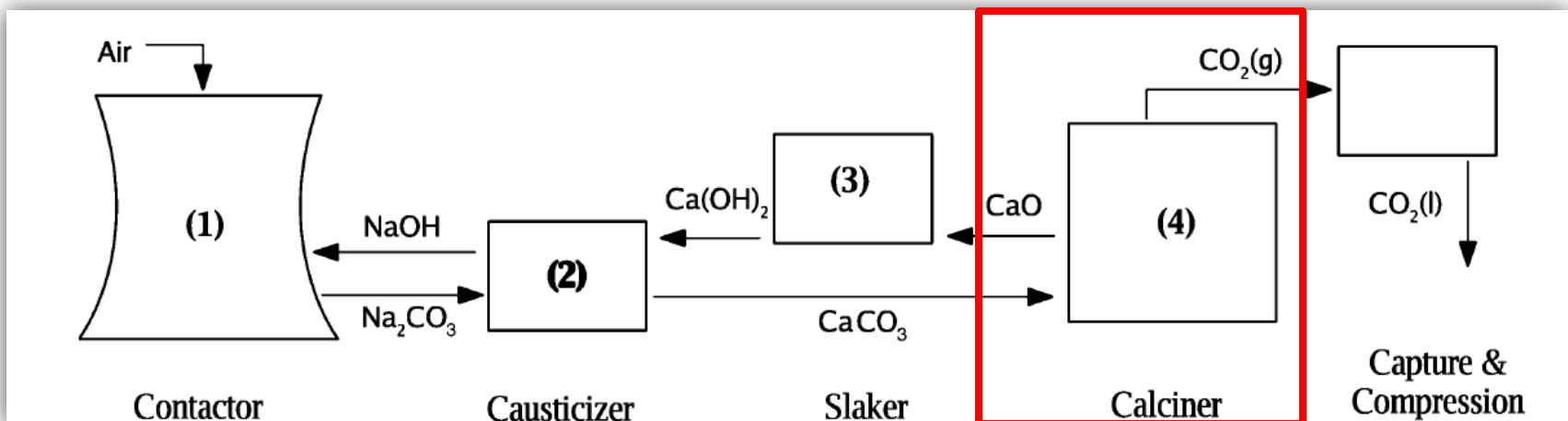


The Technology



Calciner

- Drives CO_2 out of mud
- Produces lime to return to chemical loop
- Requires a great deal of energy



The Technology

Na/Ca Capture

Example air capture system: estimated and analogous costs and energy requirements

| System | Mechanical energy (GJ/tC) | Thermal energy (GJ/tC) | Cost [\$/tC] ^a |
|---|---------------------------|------------------------|---------------------------|
| Calcination | | | |
| Calcination in lime production | 0.3 | 17 | 230 ^b |
| Calcination in Kraft process | (small) | 32 | ? |
| Calcination + caustization in Kraft Process | (small) | 40 | 373 ^c |
| CO ₂ capture and compression | | | |
| Amine capture | 0.4 ^d | 14 ^{d,e} | 49 ^{d,f} |
| CO ₂ compression | 1.6 ^d | 0 | 43 ^d |
| Contacting | | | |
| Spray tower | 1.0 | 0 | 41 ^f |
| Packed tower | 1.2 ^g | 0 | ? |

The Technology

COSTS

| BIOMASS CAPTURE | BIOMASS DRIVEN CAPTURE | METAL CARBONATE CAPTURE | INDUSTRIAL CAPTURE | PROPOSED CARBON TAX | Na/Ca SORBANT CAPTURE |
|------------------|---|---------------------------------------|----------------------|--|--------------------------------------|
| 0.1 - 28 | 160 | 30 - 32 | 160 - 260 | 26 - 58 | 240 - 550 |
| Limited by space | One time capture only Impacts on agriculture | Can only capture < 1% of US emissions | Point Source Capture | Kyoto Protocol McCain-Lieberman NCEP | Potential to capture 76kT/yr/unit |

UNITS: \$ / tonne of Carbon

What to do with CO₂?

- Sequestration – not proven
- Oilfield stimulation – current use, but small
- Use as Feedstock for Methanol Production $\text{CO}_2 + 2 \text{H}_2\text{O} \rightarrow \text{CH}_3\text{OH} + 3/2 \text{O}_2$

| Storage Parameter | Units | YEAR (Hydrogen Storage R&D Targets) | | | Methanol |
|----------------------|-----------------------|--|------|------|----------|
| | | 2007 | 2010 | 2015 | |
| Gravimetric Capacity | kWh/kg | 1.5 | 2.0 | 3.0 | 6.3 |
| | kg H ₂ /kg | 4.5% | 6.0% | 9.0% | 12.5% |
| Volumetric Capacity | kWh/L | 1.2 | 1.5 | 2.7 | 4.98 |
| | g H ₂ /L | 36 | 45 | 81 | 98.9 |

Personal Communication with Dr. Scovazzo

Conclusions*

- Using existing technologies, atmospheric CO₂ removal is feasible, but often not feasible economically
- When targeting the transportation sector, atmospheric CO₂ removal is cheapest of proposed methods
- Atmospheric CO₂ removal is not economically feasible as a replacement for point source recovery
- The research of this technology is worthwhile!

? GRT ?

* If GRT has really done what they say, the conclusions could change

Comments

- Atmospheric extraction is only one solution to the problem
- The Global Warming industry is profitable for private environmental remediation organizations
- Population must be educated
- Conservation must be instilled into upcoming generations
- Will require global effort



References

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- Lackner, Grimes, and Ziock; Capturing Carbon Dioxide from Air; White Paper
- Stolaroff, Lowry, and Keith; CO₂ Capture from the ambient air: An example system; White Paper, Carnegie Mellon University
- Stolaroff, Keith, and Lowry; Carbon Dioxide Capture from Atmospheric Air Using Sodium Hydroxide Spray; Environmental Science Technology; Feb. 2008
- Olah, Goepfert, and Prakash; Beyond Oil and Gas: The Methanol Economy; Feb. 2006
- www.grestech.com: Global Research Technologies website and press releases
- Personal communication with Dr. Paul Scovazzo

Questions?